Control system and method for adjusting CO emission levels within a boiler system
System und Verfahren zum Einstellen von CO-Emissionen in einem Dampferzeugersystem
Système et méthode pour contrôler les émissions de CO dans une chaudière

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Description

[0001] The invention is directed to a control system and a method for adjusting CO emissions within a boiler system.

BACKGROUND OF THE INVENTION

[0003] Fossil-fuel fired boiler systems have been utilized for generating electricity. One type of fossil-fuel fired boiler system combusts an air/coal mixture to generate heat energy that increases a temperature of water to produce steam. The steam is utilized to drive a turbine generator that outputs electrical power.

[0004] A by-product of combusting an oxygen and a hydrocarbon-based fuel mixture, such an air/coal mixture, is carbon monoxide (CO). One objective of a control system is to maintain total CO levels exiting a boiler system below a threshold level. The inventors herein have recognized that CO levels at particular locations in the boiler system can have CO levels greater than a threshold CO level while other locations have CO levels less than the threshold CO level. Further, the variance of CO levels in the boiler system can result in increased total CO emissions and local CO concentrations above the threshold level.

[0005] Accordingly, the inventors herein have recognized a need for an improved system and method for controlling a boiler system that can determine locations within the boiler system that have relatively high CO levels and that can adjust an air-fuel (A/F) ratio of burners affecting those locations to decrease CO levels therein.

[0006] US 4,887,958 discloses a system for controlling the supply of fuel and air to a furnace, comprising a plurality of burner assemblies, each with its own air valve for controlling the flow of combustion air therethrough. Each burner assembly is provided with a sensing instrument to sense the individual performance of the burner assembly.

[0007] US 2004/0191914 discloses a method of optimizing combustion in a fossil fuel fired boilers, wherein a plurality of carbon monoxide sensors are provided in an exit portion of a boiler furnace. Various other types of sensor are provided in the furnace. Air flow to the burners is adjusted to alleviate spatial combustion anomalies.

BRIEF DESCRIPTION OF THE INVENTION

[0008] The present invention provides a method for adjusting CO emission levels within a boiler system according to claim 1 and a control system in accordance with claim 6.

[0009] A method for adjusting CO emission levels within a boiler system in accordance with an exemplary embodiment is provided. The boiler system has a first plurality of burners and a plurality of CO sensors disposed therein. The method includes receiving a plurality of signals from the plurality of CO sensors disposed at a first plurality of locations in the boiler system. The method further includes determining a plurality of CO levels at the first plurality of locations based on the plurality of signals. The method further includes determining a second plurality of locations that have CO levels greater than or equal to a threshold CO level. The second plurality of locations is a subset of the first plurality of locations. The method further includes determining a second plurality of burners in the boiler system that are contributing to the second plurality of locations having CO levels greater than or equal to the threshold CO level. The second plurality of burners is a subset of the first plurality of burners.

[0010] A control system for adjusting CO emission levels within a boiler system in accordance with another exemplary embodiment is provided. The boiler system includes a plurality of CO sensors disposed at a first plurality of locations in the boiler system. The plurality of CO sensors are configured to generate a plurality of signals indicative of CO levels at the first plurality of locations. The control system further includes a controller operably coupled to the plurality of CO sensors. The controller is configured to receive the plurality of signals and to determine a plurality of CO levels at the first plurality of locations based on the plurality of signals. The controller is further configured to determine a second plurality of locations that have CO levels greater than or equal to a threshold CO level. The second plurality of locations are a subset of the first plurality of locations. The controller is further configured to determine a second plurality of burners in the boiler system that are contributing to the second plurality of locations having CO levels greater than or equal to the threshold CO level. The second plurality of burners is a subset of the first plurality of burners.

[0011] An article of manufacture in accordance with another exemplary embodiment is provided. The article of manufacture includes a computer storage medium.
having a computer program encoded therein for adjusting CO emission levels within a boiler system. The boiler system has a first plurality of burners and a plurality of CO sensors disposed therein. The computer storage medium includes code for receiving a plurality of signals from the plurality of CO sensors disposed at a first plurality of locations in the boiler system. The computer storage medium further includes code for determining a plurality of CO levels at the first plurality of locations based on the plurality of signals. The computer storage medium further includes code for determining a second plurality of locations that have CO levels greater than or equal to a threshold CO level. The second plurality of locations is a subset of the first plurality of locations. The computer storage medium further includes code for determining a second plurality of burners in the boiler system that are contributing to the second plurality of locations having CO levels greater than or equal to the threshold CO level. The second plurality of burners is a subset of the first plurality of burners. The computer storage medium further includes code for determining an amount of CO being generated by each burner of the first plurality of burners for each location of the second plurality of locations. The computer storage medium further includes code for increasing an A/F ratio of at least one burner of the second plurality of burners to increase A/F ratios at the second plurality of locations in order to decrease the CO levels at the second plurality of locations toward the threshold CO level, based on the amount of CO being generated by the at least one burner of the second plurality of burners.

There follows a detailed description of embodiments of the invention by way of example only with reference to the accompanying drawings, in which:

Figure 1 illustrates a power generation system having a boiler system and a control system in accordance with an exemplary embodiment;

Figure 2 is a block diagram of software algorithms utilized in the control system of Figure 1;

Figures 3-5 are flowcharts of a method for adjusting CO levels in predetermined locations of the boiler system of Figure 1;

Figure 6 is a schematic of mapped values utilized by the control system of Figure 1 for controlling burner A/F ratio values based on CO levels in the boiler system; and

Figure 7 is a schematic of a burner utilized in the boiler system of Figure 1.

DETAILED DESCRIPTION OF THE INVENTION

Referring to Figure 1, a power generation system 10 for generating electrical power is illustrated. The power generation system 10 includes a boiler system 12, a control system 13, a turbine generator 14, a conveyor 16, a silo 18, a coal feeder 20, a coal pulverizer 22, an air source 24, and a smokestack 28. The boiler system 12 is provided to burn an air-coal mixture to heat water to generate steam therefrom. The steam is utilized to drive the turbine generator 14, which generates electricity. It should be noted that in an alternative embodiment, the boiler system 12 could utilize other types of fuels, instead of coal, to heat water to generate steam therefrom. For example, the boiler system 12 could utilize any conventional type of hydrocarbon fuel such as gasoline, diesel fuel, oil, natural gas, propane, or the like. The boiler system 12 includes a furnace 40 coupled to a back path portion 42, an air intake manifold 44, burners 47, 48, 50, 52, an air port 53, and conduits 59, 60, 62, 64, 66, 68. The furnace 40 defines a region where the air-coal mixture is burned and steam is generated. The back path portion 42 is coupled to the furnace 40 and receives exhaust gases from the furnace 40. The back path portion 42 transfers the exhaust gases from the furnace 40 to the smokestack 28. The air intake manifold 44 is coupled to the furnace 40 and provides a predetermined amount of secondary air to the burners 47, 48, 50, 52 and air port 53 utilizing the throttle valves 45, 46. Further, the burners 47, 48, 50, 52 receive an air-coal mixture from the air source 24 via the conduits 60, 62, 64, 66, respectively. The burners 47, 48, 50, 52 are disposed through apertures in the furnace 40. The burners 47, 48, 50, 52 emit flames into an interior region of the furnace 40 to heat water. Because the burners 47, 48, 50, 52 have a substantially similar structure, only a detailed explanation of the structure of the burner 47 will be provided. Referring to Figure 7, the burner 47 has concentrically disposed tubes 70, 72, 74. The tube 70 receives the primary air-coal mixture (air-fuel mixture) from the conduit 60. The conduit 72 is disposed around the conduit 70 and receives secondary air from the air intake manifold 44. The conduit 74 is disposed around the conduit 72 and receives tertiary air also from the air intake manifold 44. The total air-coal mixture supplied to the burner 47 is ignited at an outlet port of the burner 47 and burned in the furnace. The burner 47 further includes a valve 75 disposed in the flow path between the tube 70 and the tube 72. An operational position of the valve 75 can be operably controlled by the controller 122 to control an amount of tertiary air being received by the burner 47. Further, the burner 47 further includes a valve 77 disposed in the flow path between the tube 72 and the tube 74. An operational position of the valve 77 can be operably controlled by the controller 122 to control an amount of secondary air being received by the burner 47. Referring to Figure 1, the control system 13 is provided to control an amount of air and coal received by the burners 47, 48, 50, 52 and air received by the air port 53. In particular, the control system 13 is provided
to control A/F ratios and air-fuel mass flows at the burners 47, 48, 50, 52 and air injection port 53 to control CO levels, temperature levels, and a rate of slag formation at predetermined locations in the boiler system 12. The control system 13 includes electrically controlled primary air and coil valves 80, 82, 84, 86, 88, a combustion air actuator 90, an overfire air actuator 92, CO sensors 94, 96, 98, 99, temperature sensors 110, 112, 114, 115, slag detection sensors 116, 118, 120, 121, mass air flow sensors 117, 119, a coal flow sensor 123, and a controller 122. It should be noted that for purposes of discussion, it is presumed that the CO sensor 94, the temperature sensor 110, and the slag detection sensor 116 are disposed substantially at a first location within the boiler system 12. Further, the CO sensor 96, the temperature sensor 112, the slag detection sensor 118 are disposed substantially at a second location within the boiler system 12. Further, the CO sensor 98, the temperature sensor 114, the slag detection sensor 120 are disposed substantially at a third location within the boiler system 12. Still further, the CO sensor 99, the temperature sensor 115, and the slag detection sensor 121 are disposed substantially at a fourth location with the boiler system 12. Of course, it should be noted that in alternative embodiments the CO sensors, temperature sensors, and slag detection sensors can be disposed in different locations with respect to one another. Further, in an alternate embodiment, the CO sensors 94, 96, 98, 99 are disposed away from the first, second, third, and fourth locations respectively in the boiler system 12 and the CO levels at the first, second, third and fourth locations are estimated from the signals of CO sensors 94, 96, 98, 99, respectively, utilizing computational fluid dynamic techniques known to those skilled in the art. Further, in an alternate embodiment, the temperature sensors 110, 112, 114, 115 are disposed away from the first, second, third, and fourth locations, respectively, and the temperature levels at the first, second, third, and fourth locations are estimated from the signals of temperature sensors 110, 112, 114, 115, respectively utilizing computational fluid dynamic techniques known to those skilled in the art. Further, in an alternate embodiment, the slag detection sensors 116, 118, 120, 121 are disposed away from the first, second, third, and fourth locations, respectively, and the slag thickness levels are estimated from the signals of the slag detection sensors 116, 118, 120, 121, respectively, utilizing computational fluid dynamic techniques known to those skilled in the art. [0018] The electrically controlled valves 80, 82, 84, 86, 88 are provided to control an amount of primary air or transport air delivered to the burners 47, 48, 50, 52 and conduit 68, respectively, in response to control signals (FV1), (FV2), (FV3), (FV4), (FV5), respectively, received from the controller 122. The primary air carries coal particles to the burners. [0019] The actuator 90 is provided to control an operational position of the throttle valve 45 in the air intake manifold 44 for adjusting an amount of combustion air provided to the burners 47, 48, 50, 52, in response to a control signal (AV1) received from the controller 122. [0020] The actuator 92 is provided to control an operational position of the throttle valve 46 for adjusting an amount of over-fire air provided to the air port 53, in response to a control signal (AV2) received from the controller 122. [0021] The CO sensors 94, 96, 98, 99 are provided to generate signals (CO1), (CO2), (CO3) (CO4) indicative of CO levels at the first, second, third, and fourth locations, respectively, within the boiler system 12. It should be noted that in an alternative embodiment, the number of CO sensors within the boiler system 12 can be greater than four CO sensors. For example, in an alternative embodiment, a bank of CO sensors can be disposed within the boiler system 12. As shown, the CO sensors 94, 96, 98, 99 are disposed in the back pass portion 42 of the boiler system 12. It should be noted that in an alternative embodiment, the CO sensors can be disposed in a plurality of other positions within the boiler system 12. For example, the CO sensors can be disposed at an exit plane of the boiler system 12. [0022] The temperature sensors 110, 112, 114, 115 are provided to generate signals (TEMP1), (TEMP2), (TEMP3), (TEMP4) indicative of temperature levels at the first, second, third and fourth locations, respectively, within the boiler system 12. It should be noted that in an alternative embodiment, the number of temperature sensors within the boiler system 12 can be greater than four temperature sensors. For example, in an alternative embodiment, a bank of temperature sensors can be disposed within the boiler system 12. As shown, the temperature sensors 110, 112, 114, 115 are disposed in the furnace exit plane portion 42 of the boiler system 12. It should be noted that in an alternative embodiment, the temperature sensors can be disposed in a plurality of other positions within the boiler system 12. For example, the temperature sensors can be disposed at an exit plane of the boiler system 12. [0023] The slag detection sensors 116, 118, 120, 121 are provided to generate signals (SLAG1), (SLAG2), (SLAG3), (SLAG4) indicative of slag thicknesses at the first, second, third, and fourth locations, respectively, within the boiler system 12. It should be noted that in an alternative embodiment, the number of slag detection sensors within the boiler system 12 can be greater than four slag detection sensors. For example, in an alternative embodiment, a bank of slag detection sensors can be disposed within the boiler system 12. As shown, the slag detection sensors 116, 118, 120, 121 are disposed in the back path portion 42 of the boiler system 12. It should be noted that in an alternative embodiment, the slag detection sensors can be disposed in a plurality of other positions within the boiler system 12. For example, the slag detection sensors can be disposed at an exit plane of the boiler system 12. [0024] The mass flow sensor 119 is provided to generate a (MAF1) signal indicative of an amount of primary
air being supplied to the conduit 59, that is received by the controller 122.

[0025] The mass flow sensor 117 is provided to generate a (MAF2) signal indicative of an amount of combustion air being supplied to the intake manifold 44 and the burners and air ports, that is received by the controller 122.

[0026] The coal flow sensor 123 is provided to generate a (CF) signal indicative of an amount of coal being supplied to the conduit 59, that is received by the controller 122.

[0027] The controller 122 is provided to generate control signals to control operational positions of the valves 80, 82, 84, 86, 88 and actuators 90, 92 for obtaining a desired A/F ratio at the burners 47, 48, 50, 52. Further, the controller 122 is provided to receive signals (CO1-CO4) from the CO sensors 94, 96, 98, 99 indicative of CO levels at the first, second, third and fourth locations and to determine the CO levels therefrom. Further, the controller 122 is provided to receive signals (TEMP1-TEMP4) from the temperature sensors 110, 112, 114, 115 indicative of temperature levels at the first, second, third, and fourth locations and to determine temperature levels therefrom. Still further, the controller 122 is provided to receive signals (SLAG1-SLAG4) from the slag detection sensors 116, 118, 120, 121 indicative of slag thicknesses at the first, second, third, and fourth locations and to determine slag thicknesses therefrom. The controller 122 includes a central processing unit (CPU) 130, a read-only memory (ROM) 132, a random access memory (RAM) 134, and an input-output (I/O) interface 136. Of course any other conventional types of computer storage media could be utilized including flash memory or the like, for example. The CPU 30 executes the software algorithms stored in at least one of the ROM 132 and the RAM 134 for implementing the control methodology described below.

[0028] Referring to Figure 2, a block diagram of the software algorithms executed by the controller 122 is illustrated. In particular, the software algorithms include a burner A/F ratio estimation module 140, a spatial A/F ratio estimation module 142, a mass flow based influence factor map 144, and a spatial CO estimation module 146.

[0029] The burner A/F ratio estimation module 140 is provided to calculate an A/F ratio at each of the burners 47, 48, 50, 52. In particular, the module 140 calculates the A/F ratio and each of the burners based upon the amount of primary air, secondary air, and tertiary air and coal being provided to be burners 47, 48, 50, 52 and an amount of coal being provided by the coal pulverizer 22.

[0030] The mass flow based influence factor map 144 comprises a table that correlates a mass flow amount of exhaust gases from each burner to each of the first, second, third, and fourth locations within the boiler system 12. The controller 122 can utilize the mass flow based influence factor map 144 to determine which burners are primarily affecting particular locations within the boiler system 12. In particular, the controller 122 can determine that a particular burner is primarily affecting a particular location within the boiler system 12 by determining that a mass flow value from the particular burner to the particular location is greater than a threshold mass flow value.

[0031] In an alternative embodiment, the mass flow based influence factor map 144 comprises a table that indicates a percentage value indicating a percentage of the mass flow from each burner that flows to each of the first, second, third, and fourth locations. The controller 122 can determine that a particular burner is primarily affecting a particular location within the boiler system 12 by determining that a percentage value associated with a particular burner and a particular location is greater than a threshold percentage value. For example, the table could indicate that 10% of the mass flow at the first location is from the burner 47. If the threshold percentage value is 5%, then the controller 122 would determine burner 47 is primarily affecting the mass flow at the first location.

[0032] The mass flow based influence factor map 144 can be determined using isothermal physical models and fluid dynamic scaling techniques of the boiler system 12 or computational fluid dynamic models of the boiler system 12.

[0033] The spatial A/F ratio estimation model 142 is provided to calculate an A/F ratio at each of the first, second, third, and fourth locations in the boiler system 12. In particular, the module 142 utilizes the A/F ratios associated with each of the burners and the mass flow based influence factor map 144 to calculate an A/F ratio at each of the first, second, third, and fourth locations in the boiler system 12.

[0034] The spatial CO estimation model 142 is provided to calculate a CO level at each of the first, second, third, and fourth locations in the boiler system 12. In particular, the module 142 utilizes the A/F ratio at each of the first, second, third, and fourth locations to estimate the CO levels at the first, second, third, and fourth locations.

[0035] Referring to Figures 3-5, a method for adjusting CO levels in the boiler system 12 will now be explained. The method can be implemented utilizing software algorithms executed by the controller 122.

[0036] At step 150, a first plurality of CO sensors disposed at a first plurality of locations, respectively, in a boiler system 12 generate a first plurality of signals, respectively, indicative of CO levels at the first plurality of locations. For example, the CO sensors 94, 96, 98, 99 can generate signals (CO1), (CO2), (CO3), (CO4) respectively, indicative of CO levels at the first, second, third, and fourth locations, respectively.

[0037] At step 152, the controller 122 receives the first plurality of signals and determines a first plurality of CO levels associated with the first plurality of locations. For example, the controller 122 can receive the signals (CO1), (CO2), (CO3) (CO4) and determine CO levels associated with the first, second, third, and fourth loca-
At step 154, the controller 122 determines a second plurality of locations comprising a subset of the first plurality of locations, that have CO levels greater than or equal to a threshold CO level. For example, the controller 122 can determine that the first and second locations have CO levels greater than or equal to the threshold CO level.

At step 156, the controller 122 determines a third plurality of locations comprising a subset of the first plurality of locations, that have CO levels less than the threshold CO level. For example, the controller 122 can determine that the third and fourth locations have CO levels less than the threshold CO level.

At step 158, the air flow sensor 119 generates the (MAF1) signal indicative of a primary air mass flow entering the boiler system 12, that is received by the controller 122.

At step 159, the air flow sensor 117 generates the (MAF2) signal indicative of a combustion air mass flow entering the intake manifold 44, that is received by the controller. The combustion air mass flow comprises the secondary air and tertiary air received by the burners and the overfire air received by the air port 53.

At step 160, the coal flow sensor 123 generates the (CF) signal indicative of an amount of coal (e.g., total mill coal flow) entering the boiler system 12, that is received by the controller 122. Of course, in an alternate embodiment, the amount of coal being received by each burner can be calculated or monitored using coal flow sensors.

At step 162, the controller 122 executes the burner A/F ratio calculation module 140 to determine an A/F ratio of each of the first plurality of burners in the boiler system 12 based on the (MAF1) signal, the (MAF2) signal, and the (CF) signal. For example, the controller 122 can execute the burner A/F ratio calculation module 140 to determine A/F ratios for the burners 47, 48, 50, 52 based on the (MAF1) signal, the (MAF2) signal, and the (CF) signal. After step 162, the controller 122 substantially simultaneously executes both sets of steps 164-168 and steps 170-174.

Referring to Figure 4, the steps 164-168 will now be explained. At step 164, the controller 122 executes the spatial A/F ratio estimation module 142 that utilizes the mass flow based influence factor map 144, to determine an A/F ratio at each of the second plurality of locations, based on the A/F ratio at each of the first plurality of burners, and to determine a second plurality of burners comprising a subset of the first plurality of burners that are primarily influencing the CO levels at the second plurality of locations. For example, the controller 122 can execute the module 142 the utilizes the mass flow based influence factor map 144 to determine A/F ratios at the first and second locations, based on the A/F ratio at each of the burners 47, 48, 50, 52. Further, for example, the controller 122 can determine that the burners 47, 48 are primarily influencing the CO levels at the first and second locations in the boiler system 12. After step 164, the method advances to step 166.

At step 166, the controller 122 executes a spatial CO estimation module 146 to estimate an amount of CO being generated by each of the first plurality of burners at each of the second plurality of locations in the boiler system 12. For example, the controller 122 can execute the module 146 to estimate an amount of CO being generated by the burners 47, 48, 50, 52 at the first and second locations in the boiler system 12. After step 166, the method advances to step 168.

At step 168, the controller 122 increases an A/F ratio of at least one burner of the second plurality of burners, based on the amount of CO being generated by at least one burner of the second plurality burners, to adjust the CO levels at the second plurality of locations toward the threshold CO level. For example, the controller 122 can increase an A/F ratio of at least one of the burners 47, 48, based on the amount of CO being generated by at least one of burners 47, 48, to adjust CO levels at first and second locations toward the threshold CO level by increasing a fuel mass-flow into at least one of burners 47, 48 while maintaining or decreasing an air mass-flow to the at least one of burners 47, 48. Referring to Figure 6, the controller 122 can utilize a table or transfer function illustrated by the waveform 180 to determine a desired A/F ratio or an A/F ratio adjustment value for the burners 47, 48 based on a measured CO level. After step 168, the method returns to step 150.

Referring to Figure 5, the steps 170-174 will now be explained. At step 170, the controller 122 executes the spatial A/F ratio estimation module 142 that utilizes the mass-flow based influence factor map 144, to determine an A/F ratio at each of the third plurality of locations, based on the A/F ratio at each of the first plurality of burners, and to determine a third plurality of burners comprising a subset of the first plurality of burners that are primarily influencing the CO levels at the third plurality of locations. For example, the controller 122 can execute the module 142 the utilizes the mass flow based influence factor map 144 to determine A/F ratios at the third and fourth locations, based on the A/F ratio at each of the burners 47, 48, 50, 52. Further, for example, the controller 122 can determine that the burners 50, 52 are primarily influencing the CO levels at the third and fourth locations in the boiler system 12. After step 170, the method advances to step 172.

At step 172, the controller executes the spatial CO estimation module 146 to estimate an amount of CO being generated by each of the first plurality of burners at each of the third plurality of locations in the boiler system 12. For example, the controller 122 can execute the module 146 to estimate an amount of CO being generated by the burners 47, 48, 50, 52 at the third and fourth locations in the boiler system 12. After step 172, the method advances to step 174.

At step 174, the controller 122 decreases an A/F ratio of at least one burner of the third plurality of...
burners, based on the amount of CO being generated by at least one burner of the third plurality burners, while maintaining CO levels at the third plurality of locations less than or equal to the threshold CO level. For example, the controller 122 can decrease an A/F ratio of at least one of the burners 50, 52 based on a measured CO level. After step 174, the method returns to step 150.

The inventive system, method, and article of manufacture for adjusting CO levels provide a substantial advantage over other system and methods. In particular, these embodiments provide a technical effect of adjusting A/F ratios at burners to decrease CO levels at predetermined locations in a boiler system that are greater than a threshold CO level to improve outputted CO emission levels.

The above-described methods can be embodied in the form of computer program code containing instructions embodied in tangible media, such as floppy diskettes, CD ROMs, hard drives, or any other computer-readable storage medium, wherein, when the computer program code is loaded into and executed by a computer, the computer becomes an apparatus for practicing the invention.

Claims

1. A method for adjusting CO emission levels within a boiler system (12), the boiler system (12) having a first plurality of burners (47, 48, 50, 52) and a plurality of CO sensors (94, 96, 98, 99) disposed therein, the method comprising:

receiving a plurality of signals from the plurality of CO sensors (94, 96, 98, 99) disposed at a first plurality of locations in the boiler system (12) remote from the first plurality of burners;

determining a plurality of CO levels at the first plurality of locations based on the plurality of signals;

determining a second plurality of locations that have CO levels greater than or equal to a threshold CO level, the second plurality of locations being a subset of the first plurality of locations; and

determining an amount of CO being generated by each burner of the first plurality of burners (47, 48, 50, 52) for each location of the second plurality of locations in order to decrease the CO levels at the second plurality of locations toward the threshold CO level, based on the amount of CO being generated by each burner of the first plurality of burners (94, 96, 98, 99) for each location of the second plurality of locations.

accessing a mass-flow based influence factor map (144) indicating a mass flow amount or a percentage mass flow at each location of the second plurality of locations from each burner of the first plurality of burners (94, 96, 98, 99); and

identifying burners from the first plurality of burners (94, 96, 98, 99) having a mass flow amount or a percentage mass flow greater than a predetermined value, to determine the second plurality of burners.

2. The method of claim 1, wherein determining the second plurality of burners in the boiler system (12) that are contributing to the second plurality of locations having CO levels greater than or equal to the threshold CO level, comprises:

accessing a mass-flow based influence factor map (144) indicating a mass flow amount or a percentage mass flow at each location of the second plurality of locations from each burner of the first plurality of burners (94, 96, 98, 99); and

identifying burners from the first plurality of burners (94, 96, 98, 99) having a mass flow amount or a percentage mass flow greater than a predetermined value, to determine the second plurality of burners.

3. The method of claim 1 or 2, wherein increasing the A/F ratio of at least one burner of the second plurality of burners includes decreasing a fuel mass flow into the at least one burner of the second plurality of burners while maintaining or decreasing an air mass flow being delivered to the at least one burner of the second plurality of burners.
4. The method of any of the preceding claims, further comprising:

determining a third plurality of locations that have a CO level less than the threshold CO level, the third plurality of locations being a subset of the first plurality of locations;

determining a third plurality of burners in the boiler system (12) that are contributing to the third plurality of locations having CO levels less than the threshold CO level, the third plurality of burners being a subset of the first plurality of burners (94, 96, 98, 99) exclusive of the second plurality of burners;

determining an amount of CO being generated by each burner of the first plurality of burners (94, 96, 98, 99) for each location of the third plurality of locations exclusive of the second plurality of locations; and

decreasing an A/F ratio of at least one burner of the third plurality of burners while maintaining CO levels at the third plurality of locations less than the threshold CO level, based on the amount of CO being generated by the at least one burner of the third plurality of burners.

5. The method of claim 4, wherein decreasing the A/F ratio of at least one burner of the third plurality of burners includes increasing a fuel mass flow into the at least one burner of the third plurality of burners while maintaining or decreasing an air mass flow delivered to the at least one burner of the third plurality of burners.

6. A control system (13) for adjusting CO emission levels within a boiler system (12), the boiler system (12) having a first plurality of burners (47, 48, 50, 52), the system comprising:

a plurality of CO sensors (94, 96, 98, 99) disposed at a first plurality of locations in the boiler system (12) remote from the first plurality of burners (47, 48, 50, 52), the plurality of CO sensors (94, 96, 98, 99) configured to generate a plurality of signals indicative of CO levels at the first plurality of locations; and

a controller (122) operably coupled to the plurality of CO sensors (94, 96, 98, 99), the controller (122) configured to receive the plurality of signals and to determine a plurality of CO levels at the first plurality of locations based on the plurality of signals, the controller (122) further configured to determine a second plurality of locations that have CO levels greater than or equal to a threshold CO level, the second plurality of locations being a subset of the first plurality of locations, the controller (122) further configured to determine a second plurality of burners in the boiler system (12) that are contributing to the second plurality of locations having CO levels greater than or equal to the threshold CO level, the second plurality of burners being a subset of the first plurality of burners (47, 48, 50, 52), the controller (122) further configured to determine an amount of CO being generated by each burner of the first plurality of burners (94, 96, 98, 99) for each location of the second plurality of locations, and the controller (122) is further configured to determine an A/F ratio of each burner of the first plurality of burners (94, 96, 98, 99), the controller (122) being further configured to determine an A/F ratio at each of the second plurality of locations based on the A/F ratio of each burner of the first plurality of burners (94, 96, 98, 99) having a mass flow amount or a percentage mass flow greater than a predetermined value, to determine the second plurality of burners.

7. The control system (13) of claim 6, wherein the controller (122) is further configured to access a mass-flow based influence factor map (144) indicating a mass flow amount or a percentage mass flow at each location of the second plurality of locations from each burner of the first plurality of burners (94, 96, 98, 99), the controller (122) being further configured to identify burners from the first plurality of burners (94, 96, 98, 99) having a mass flow amount or a percentage mass flow greater than a predetermined value, to determine the second plurality of burners.

8. The control system (13) of claim 6 or 7, wherein the controller (122) is further configured to decrease a fuel mass flow into the at least one burner of the second plurality of burners while maintaining or decreasing an air mass flow being delivered to the at least one burner of the second plurality of burners.

Patentansprüche

1. Verfahren zum Einstellen von CO-Emissionspegeln in einem Kesselsystem (12), wobei das Kesselsystem (12) mehrere erste Brenner (47, 48, 50, 52) und mehrere darin angeordnete CO-Sensoren (94,
Empfangen mehrerer Signale aus den mehreren CO-Sensoren (94, 96, 98, 99), die an mehreren Stellen in dem Kesselsystem (12) entfernt von den mehreren ersten Brennern angeordnet sind;
Ermitteln mehrerer CO-Pegel an den mehreren ersten Stellen auf der Basis der mehreren Signale;
Ermitteln mehrerer zweiter Stellen, die höhere CO-Pegel als ein oder gleich einem Schwellenwert-CO-Pegel haben, wobei die mehreren zweiten Stellen eine Untergruppe von den mehreren ersten Stellen sind;
Ermitteln mehrerer zweiter Brenner in dem Kesselsystem (12), die zu den mehreren zweiten Stellen mit CO-Pegeln größer als der oder gleich dem Schwellenwert-CO-Pegel beitragen, wobei die mehreren zweiten Brenner eine Untergruppe von den mehreren ersten Brennern (47, 48, 50, 52) sind;
Ermitteln einer CO-Menge, die durch jeden Brenner von den mehreren ersten Brennern (47, 48, 50, 52) für jede Stelle von den mehreren zweiten Stellen erzeugt wird; und
Erhöhen eines A/F-Verhältnisses wenigstens eines Brenners von den mehreren zweiten Brennern, um die A/F-Verhältnisse an den mehreren zweiten Stellen zu erhöhen, um die CO-Werte an den mehreren zweiten Stellen auf den Schwellenwert-CO-Pegel auf der Basis der CO-Menge zu verringern, die durch jeden Brenner von den mehreren zweiten Brennern erzeugt und, wobei die Ermittlung der CO-Menge, die durch jeden Brenner von den mehreren ersten Brennern (94, 96, 98, 99) für jede Stelle von den mehreren zweiten Stellen erzeugt wird, die Schritte aufweist:
Ermitteln eines A/F-Verhältnisses jedes Brenners von den mehreren ersten Brennern (94, 96, 98, 99);
Ermitteln eines A/F-Verhältnisses an jeder von den mehreren zweiten Stellen auf der Basis des A/F-Verhältnisses jedes Brenners von den mehreren ersten Brennern (94, 96, 98, 99); und
Ermitteln einer CO-Menge, die durch jeden Brenner von den mehreren ersten Brennern (94, 96, 98, 99) für jede Stelle von den mehreren zweiten Brennern erzeugt wird, auf der Basis des A/F-Verhältnisses jeder Stelle von den mehreren zweiten Stellen.

2. Verfahren nach Anspruch 1, wobei die Ermittlung der mehreren zweiten Brenner des Kesselsystems (12), die zu den mehreren zweiten Stellen mit CO-Pegeln größer als der oder gleich dem Schwellenwert-CO-Pegel beitragen, die Schritte aufweist:

Zugreifen auf ein Massenstrom-basiierendes Einflussfaktorkennfeld (144), das eine Massenstrommenge oder einen prozentualen Massenstrom an jeder Stelle von den mehreren zweiten Stellen aus jedem Brenner von den mehreren ersten Brennern (94, 96, 98, 99) anzeigt; und


4. Verfahren nach einem der vorstehenden Ansprüche, ferner mit den Schritten:

Ermitteln mehrerer dritter Stellen, die einen CO-Pegel haben, der kleiner als der Schwellenwert-CO-Pegel ist, wobei die mehreren dritten Stellen eine Untergruppe von den mehreren ersten Stellen sind;
Ermitteln mehrerer dritter Brenner in dem Kesselsystem (12), die zu den mehreren dritten Stellen mit CO-Pegeln kleiner als der Schwellenwert-CO-Pegel beitragen, wobei die mehreren dritten Brenner eine Untergruppe von den mehreren ersten Brennern (94, 96, 98, 99) ausgeschließlich der mehreren zweiten Brenner sind;
Ermitteln einer CO-Menge, die durch jeden Brenner von den mehreren ersten Brennern (94, 96, 98, 99) für jede Stelle von den mehreren dritten Stellen ausschließlich einer mehreren zweiten Stelle erzeugt wird; und

5. Verfahren nach Anspruch 4, wobei das Verringern des A/F-Verhältnisses wenigstens eines Brenners

...

mehrere CO-Sensoren (94, 96, 98, 99), die an mehreren ersten Stellen in dem Kesselsystem (12) anordnet sind, wobei die mehreren CO-Sensoren (94, 96, 98, 99) dafür eingerichtet sind, mehrere Signale zu erzeugen, die CO-Pegel an den mehreren ersten Stellen anzeigen; und

7. Steuerungssystem (13) nach Anspruch 6, wobei die Steuerung (122) dafür eingerichtet ist, auf einer Massenstrom-basierenden Einflussfaktorkennfeld (144) zuzugreifen, das eine Massenstrommenge oder einen prozentualen Massenstrom an jeder Stelle von den mehreren zweiten Stellen aus jedem Brenner von den mehreren ersten Brennern (94, 96, 98, 99) anzeigt, wobei die Steuerung (122) für jedes Brennern von den mehreren ersten Stellen (94, 96, 98, 99) mit einer Massenstrommenge oder einem prozentualen Massenstrom größer als ein vorbestimmter Wert zu identifizieren, um die mehreren zweiten Brenner zu ermitteln.


Revidendations

1. Procédé pour régler des niveaux d’émission de CO dans un système de chaudière (12), le système de chaudière (12) ayant une première pluralité de brûleurs (47, 48, 50, 52) et une pluralité de détecteurs de CO (94, 96, 98, 99) disposés dans celui-ci, le procédé comportant :

la réception d’une pluralité de signaux émis par la pluralité de détecteurs de CO (94, 96, 98, 99) disposés, dans le système de chaudière (12), en une première pluralité d’endroits distants de la première pluralité de brûleurs ;
déterminer, d’après la pluralité de signaux, une pluralité de niveaux de CO en la première pluralité d’endroits ;
déterminer une deuxième pluralité d’endroits où le niveau de CO est supérieur ou égal à un ni-
veau seuil de CO, la deuxième pluralité d’endroits étant un sous-ensemble de la première pluralité d’endroits ;

déterminer une deuxième pluralité de brûleurs du système de chaudière (12) qui contribuent à la deuxième pluralité d’endroits où le niveau de CO est supérieur ou égal au niveau seuil de CO, la deuxième pluralité de brûleurs étant un sous-ensemble de la première pluralité de brûleurs (47, 48, 50, 52) ;

déterminer une quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (47, 48, 50, 52) pour chaque endroit de la deuxième pluralité d’endroits ; et

accroître une richesse de mélange d’au moins un brûleur de la deuxième pluralité de brûleurs afin d’accroître la richesse du mélange en la deuxième pluralité d’endroits afin d’abaisser vers le niveau seuil de CO le niveau de CO en la deuxième pluralité d’endroits d’après la quantité de CO produite par le/les brûleur(s) de la deuxième pluralité de brûleurs, la détermination de la quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99) pour chaque endroit de la deuxième pluralité d’endroits comprenant :

la détermination d’une richesse de mélange de chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99) ;

la détermination, d’après la richesse du mélange de chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99), d’une richesse de mélange en chaque endroit de la deuxième pluralité d’endroits ; et

la détermination, d’après la richesse du mélange en chaque endroit de la deuxième pluralité d’endroits, d’une quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99) pour chaque endroit de la deuxième pluralité d’endroits.

2. Procédé selon la revendication 1, dans lequel la détermination de la deuxième pluralité de brûleurs du système de chaudière (12) qui contribuent à la deuxième pluralité d’endroits où le niveau de CO est supérieur ou égal au niveau seuil de CO comprend :

l’accès, depuis chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99), à une carte (144) de facteurs d’influence reposant sur le débit massique, indiquant une valeur de débit massique ou un pourcentage de débit massique en chaque endroit de la deuxième pluralité d’endroits ; et

l’identification, parmi la première pluralité de brûleurs (94, 96, 98, 99), de brûleurs ayant une valeur de débit massique ou un pourcentage de débit massique supérieur à une valeur prédéterminée, afin de déterminer la deuxième pluralité de brûleurs.

3. Procédé selon la revendication 1 ou 2, dans lequel l’accroissement de la richesse du mélange d’au moins un brûleur de la deuxième pluralité de brûleurs comprend la réduction d’un débit massique de combustible vers le/les brûleur(s) de la deuxième pluralité de brûleurs tout en maintenant ou en réduisant un débit massique d’air fourni au(x) brûleur(s) de la deuxième pluralité de brûleurs.

4. Procédé selon l’une quelconque des revendications précédentes, comportant en outre :

la détermination d’une troisième pluralité d’endroits où le niveau de CO est inférieur au niveau seuil de CO, la troisième pluralité d’endroits étant un sous-ensemble de la première pluralité d’endroits ;

la détermination d’une troisième pluralité de brûleurs du système de chaudière (12) qui contribuent à la troisième pluralité d’endroits où le niveau de CO est inférieur au niveau seuil de CO, la troisième pluralité de brûleurs étant un sous-ensemble de la première pluralité de brûleurs (94, 96, 98, 99) excluant la deuxième pluralité de brûleurs ;

la détermination d’une quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99) pour chaque endroit de la troisième pluralité d’endroits excluant la deuxième pluralité d’endroits ; et

la réduction d’une richesse de mélange d’au moins un brûleur de la troisième pluralité de brûleurs tout en maintenant le niveau de CO en la troisième pluralité d’endroits au-dessous du niveau seuil de CO, d’après la quantité de CO produite par le/les brûleur(s) de la troisième pluralité de brûleurs.

5. Procédé selon la revendication 4, dans lequel la réduction de la richesse du mélange d’au moins un brûleur de la troisième pluralité de brûleurs comprend l’augmentation d’un débit massique de combustible vers le/les brûleur(s) tout en maintenant ou en réduisant un débit massique d’air fourni au(x) brûleur(s) de la troisième pluralité de brûleurs.

6. Système de commande (13) pour régler des niveaux d’émission de CO dans un système de chaudière (12), le système de chaudière (12) ayant une première pluralité de brûleurs (47, 48, 50, 52), le système comportant :

une pluralité de détecteurs de CO (94, 96, 98,
99) disposés, dans le système de chaudière (12), en une première pluralité d’endroits distants de la première pluralité de brûleurs (47, 48, 50, 52), la pluralité de détecteurs de CO (94, 96, 98, 99) étant conçus pour produire une pluralité de signaux indiquant le niveau de CO en la première pluralité d’endroits ; et un moyen de commande (122) coopérant avec la pluralité de détecteurs de CO (94, 96, 98, 99), le moyen de commande (122) étant conçu pour recevoir la pluralité de signaux et déterminer, d’après la pluralité de signaux, une pluralité de niveaux de CO en la première pluralité d’endroits, le moyen de commande (122) étant en outre conçu pour déterminer une deuxième pluralité d’endroits où le niveau de CO est supérieure ou égal à un niveau seuil de CO, la deuxième pluralité d’endroits étant un sous-ensemble de la première pluralité d’endroits, le moyen de commande (122) étant en outre conçu pour déterminer une deuxième pluralité de brûleurs du système de chaudière (12) qui contribuent à la deuxième pluralité d’endroits où le niveau de CO est supérieur ou égal au niveau seuil de CO, la deuxième pluralité de brûleurs étant un sous-ensemble de la première pluralité de brûleurs (47, 48, 50, 52), le moyen de commande (122) étant en outre conçu pour accroître une richesse de mélange d’au moins un brûleur de la deuxième pluralité de brûleurs afin d’accroître la richesse du mélange en la deuxième pluralité d’endroits dans le but d’abaisser, vers le niveau seuil de CO, le niveau de CO en la deuxième pluralité d’endroits, d’après la quantité de CO produite par le/les brûleur(s) de la deuxième pluralité de brûleurs, caractérisé en ce que le moyen de commande (122) est conçu pour déterminer une quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (47, 48, 50, 52) pour chaque endroit de la deuxième pluralité d’endroits, et le moyen de commande (122) est en outre conçu pour déterminer une richesse de mélange de chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99), le moyen de commande (122) étant en outre conçu pour déterminer une richesse de mélange en chaque endroit de la deuxième pluralité d’endroits d’après la richesse de mélange de chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99), le moyen de commande (122) étant en outre conçu pour déterminer une quantité de CO produite par chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99) pour chaque endroit de la deuxième pluralité d’endroits, d’après la richesse du mélange en chaque endroit de la deuxième pluralité d’endroits.

7. Système de commande (13) selon la revendication 6, dans lequel le moyen de commande (122) est en outre conçu pour accéder, depuis chaque brûleur de la première pluralité de brûleurs (94, 96, 98, 99), à une carte (144) de facteurs d’influence reposant sur le débit massique, indiquant une valeur de débit massique ou un pourcentage de débit massique en chaque endroit de la deuxième pluralité d’endroits, le moyen de commande (122) étant en outre conçu pour identifier, parmi la première pluralité de brûleurs (94, 96, 98, 99), des brûleurs ayant une valeur de débit massique ou un pourcentage de débit massique supérieur à une valeur prédéterminée, afin de déterminer la deuxième pluralité de brûleurs.

8. Système de commande (13) selon la revendication 6 ou 7, dans lequel le moyen de commande (122) est en outre conçu pour réduire un débit massique de combustible vers le/les brûleur(s) de la deuxième pluralité de brûleurs tout en maintenant ou en réduisant un débit massique d’air fourni au(x) brûleur(s) de la deuxième pluralité de brûleurs.
FIG. 2

Controller

Burner A/F Ratio Estimation Module

Spatial A/F Ratio Estimation Module

Mass-flow Based Influence Factor Map

Spatial CO Estimation Module

122

140

142

144

146
FIG. 3

Start

First plurality of CO sensors disposed at a first plurality of locations, respectively, in a boiler system generate a first plurality of signals, respectively, indicative of CO levels at the first plurality of locations

Controller receives the first plurality of signals and determines a first plurality of CO levels associated with the first plurality of locations

Controller determines a second plurality of locations comprising a subset of the first plurality of locations, that have CO levels greater than or equal to a threshold CO level

Controller determines a third plurality of locations comprising a subset of the first plurality of locations, that have CO levels less than the threshold CO level

First air flow sensor generates a second signal indicative of a primary air mass flow entering the boiler system, that is received by the controller

Second air flow sensor generates a third signal indicative of a combustion air mass flow entering an intake manifold of the boiler system, that is received by the controller

Coal flow sensor generates a fourth signal indicative of an amount of coal entering the boiler system, that is received by the controller

Controller executes a burner A/F ratio calculation module to determine an A/F ratio of each of the first plurality of burners in the boiler system based on the second, third, and fourth signals
Controller executes a spatial A/F ratio estimation module that utilizes a mass flow based influence factor map, to determine an A/F ratio at each of the second plurality of locations, based on the A/F ratio at each of the first plurality of burners, and to determine a second plurality of burners comprising a subset of the first plurality of burners that are primarily influencing the CO levels at the second plurality of locations.

Controller executes a spatial CO estimation module to estimate an amount of CO being generated by each of the first plurality of burners at each of the second plurality of locations in the boiler system.

Controller increases an A/F ratio of at least one burner of the second plurality of burners, based on the amount of CO being generated by at least one burner of the second plurality burners, to adjust the CO levels at the second plurality of locations toward the threshold CO level.
FIG. 5

Controller executes a spatial A/F ratio estimation module that utilizes the mass-flow based influence factor map, to determine an A/F ratio at each of the third plurality of locations, based on the A/F ratio at each of the first plurality of burners, and to determine a third plurality of burners comprising a subset of the first plurality of burners that are primarily influencing the CO levels at the third plurality of locations.

Controller executes a spatial CO estimation module to estimate an amount of CO being generated by each of the first plurality of burners at each of the third plurality of locations in the boiler system.

Controller decreases an A/F ratio of at least one burner of the third plurality of burners, based on the amount of CO being generated by at least one burner of the third plurality burners, while maintaining CO levels at the third plurality of locations less than or equal to the threshold CO level.
REFERENCES CITED IN THE DESCRIPTION

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