CONVENTION

AUSTRALIA

Patents Act 1990

REQUEST FOR A STANDARD PATENT

AND NOTICE OF ENTITLEMENT

The Applicant identified below requests the grant of a patent to the nominated person identified below for an invention described in the accompanying standard complete patent specification.

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[54] Invention Title:

PROCESS FOR PRODUCING SOLID ORGANO-ALUMINOXY COMPOUNDS USEFUL IN POLYMERIZATION CATALYSTS

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[31,33,32]

Details of basic application(s):

017,207 UNITED STATES OF AMERICA US 12 February 1993

Applicant states the following:

1. The nominated person is the assignee of the actual inventor(s)

2. The nominated person is
   - the applicant
   - the assignee of the applicant
   - authorised to make this application by the applicant of the basic application.

3. The basic application(s) was/were the first made in a convention country in respect of the invention.

The nominated person is not an opponent or eligible person described in Section 33-36 of the Act.

3 February 1994

Phillips Petroleum Company
By PHILLIPS ORMONDE & FITZPATRICK
Patent Attorneys
By

Our Ref : 356203

5999q
In accordance with the present invention there is provided a new solid aluminoxy composition prepared by reacting aluminoxane with a boroxine. Still further there is provided olefin polymerization catalyst systems incorporating the inventive solid aluminoxy composition. Still further, there is provided processes of polymerization using the inventive solid aluminoxy composition.
AUSTRALIA

Patents Act

COMPLETE SPECIFICATION
(ORIGINAL)

Class    Int. Class

Application Number: Lodged:

Complete Specification Lodged:
   Accepted:
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Priority

Related Art:

Name of Applicant:
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Invention Title:

PROCESS FOR PRODUCING SOLID ORGANO-ALUMINOXY COMPOUNDS
USEFUL IN POLYMERIZATION CATALYSTS

Our Ref: 356203
POF Code: 1422/50647

The following statement is a full description of this invention, including the best method of performing it known to applicant(s):

-1-
The present invention relates to aluminoxy products. The term organo-aluminoxy as used herein refers to organic compounds having a plurality of aluminum atoms each bound to at least two oxygen atoms.

In another aspect, the present invention relates to a method of modifying organic aluminoxanes to make them suitable for use in particle form polymerization. In still another aspect, the present invention relates to a metallocene catalyst comprising a modified organic aluminoxane. In still another aspect, the present invention relates to a process for polymerizing olefins using the modified organic aluminoxane.

Organic aluminoxanes are one form of aluminoxy compound. Organic aluminoxanes can be produced by the partial hydrolysis of hydrocarbyl aluminum compounds. Such aluminoxanes have been found useful in a variety of chemical reactions, including utility as catalyst components for polymerization catalysts, especially in high activity metallocene catalyst systems.

The combination of such aluminoxanes with metallocenes has been shown to be useful for certain types of olefin polymerization. One of the earliest patents containing such a disclosure is U.S. 3,242,099.

Such metallocene catalysts have been used in homogeneous solution polymerization. Since such homogeneous catalyst systems are soluble in the
polymerization medium it is generally observed that the resulting polymer has low bulk density. Further, attempts to use metallocene/aluminoxane catalysts in a slurry or particle form type polymerization have not heretofore been found to be commercially feasible. In slurry or particle form polymerization, the polymerization conditions are selected such that the polymer forms as discrete particles which are insoluble in the polymerization reaction medium during the polymerization. It has been observed that when such particle form polymerizations are carried out in the presence of a metallocene/aluminoxane catalyst system, large amounts of polymeric material are formed on the surfaces of the polymerization vessel. This fouling is particularly detrimental in a particle form process since it produces an adverse effect on the heat transfer and also results in the need for periodic if not continuous cleaning of the reactor. In order to have a metallocene/aluminoxane catalyst useful in a commercial continuous particle form process such as those using a loop reactor, it is necessary to have a catalyst system which will not cause significant amounts of reactor fouling.

It is known that a solid form of aluminoxane can be obtained by treating a commercial organo-aluminoxane solution with a countersolvent; however, even that solid has been found to cause reactor fouling in slurry polymerizations. Even when a countersolvent is used to precipitate the aluminoxane onto an insoluble particulate carrier reactor fouling is still a problem in slurry, i.e., particle form polymerization.

In accordance with the present invention a solid organo-aluminoxy product is produced by reacting an organic aluminoxane with an organic boroxine selected from the group consisting of organo-boroxines. In accordance with another aspect of the
present invention there is provided a process for the polymerization of olefins using the new organo-
aluminoxy composition as the cocatalyst, especially in particle form polymerizations.

In accordance with another aspect of the present invention a catalyst system suitable for the polymerization of olefins is produced by combining the new organo-aluminoxy composition with a transition metal based olefin polymerization catalyst.

In accordance with still another aspect of the present invention there is provided a relatively stable solid olefin polymerization catalyst comprising a metallocene and the inventive solid aluminoxy composition.

In accordance with still another aspect of the present invention there is provided a process for producing polyolefins comprising contacting at least one olefin under suitable conditions with a catalyst system comprising a suitable catalyst and the inventive organo-aluminoxy composition.

In accordance with yet another aspect of the present invention there is provided a method for making this new organo-aluminoxy composition.

In accordance with still another aspect of the invention there is provided the new organo-
aluminoxy composition resulting from the reaction of aluminoxane with the boroxine.

In accordance with yet another aspect of the present invention there is provided a solid organo-
aluminoxy composition having a surface area greater than that of the solid resulting from the vacuum stripping of an aluminoxane solution. Inventive solids having a surface area as high as 300 m$^2$/g as determined by a BET test have been prepared.

Figure 1 is a graph showing an IR spectrum of the solid resulting when the solvent is vacuum stripped from a commercial methylluminoxane solution.
Figure 2 is a graph showing an IR spectrum of a solid produced by reacting a commercial methylaluminoxane solution with methoxy boroxine.

Figure 3 is a graph showing a $^{13}$C-NMR spectra of the solid resulting from the reaction of a commercial methylaluminoxane with methoxy boroxine.

Figure 4 is a graph showing a $^{13}$C-NMR spectra of the solid resulting from vacuum stripping a commercial methylaluminoxane solution.

In accordance with the present invention, organic aluminoxanes are modified to produce a new organo-aluminoxy composition that can be used as a cocatalyst in a particle form polymerization without causing significant fouling of the polymerization reaction vessel.

Various techniques are known for making organic aluminoxanes. One technique involves the controlled addition of water to a trialkylaluminum. Another technique involves combining a trialkylaluminum and a hydrocarbon with a compound containing water of adsorption or a salt containing water of crystallization. The present invention is considered applicable to any of the commercially available organic aluminoxanes that are soluble in a hydrocarbon.

The exact structure of organic aluminoxanes is often the subject of much discussion between scholars. It is generally accepted that the aluminoxanes are oligomeric, linear and/or cyclic hydrocarbyl aluminoxanes having repeating units of the formula

$$\{O\text{-}Al\}$$

$$\mid$$

$$R$$

Typically the linear aluminoxanes are said to contain oligomers of the formula:
The oligomeric, cyclic aluminoxanes are generally viewed as having the formula:

\[
\begin{array}{c}
\text{R} - (\text{Al}-\text{O})_n - \text{AlR}_2 \\
\text{R}
\end{array}
\]

In the above formulas, \( \text{R} \) is a hydrocarbyl group, typically a \( \text{C}_1-\text{C}_8 \) alkyl group, and \( n \) is typically 2 to 50, preferably 4 to 40, \( m \) is typically 3 to 50, preferably 4 to 40. Generally, the aluminoxanes are more active as polymerization catalysts when \( m \) and \( n \) are greater than 4, more preferably at least about 10. Typically in the aluminoxanes used in the polymerization of olefins \( \text{R} \) is predominantly methyl or ethyl. Preferably at least about 30 mole percent of the repeating groups have an \( \text{R} \) which is methyl, more preferably at least 50 mole percent, and still more preferably at least 70 mole percent of the repeating units have methyl as the \( \text{R} \) group.

Some experts believe that the resulting oligomeric aluminoxane products have some significant amounts of unreacted yet somehow strongly bonded trialkylaluminums associated therewith. Among some researchers there has even been the theory that perhaps the trialkylaluminums associated with the aluminoxane is actually the material which causes the aluminoxane to be effective as a cocatalyst with metallocenes and other transition metal olefin polymerization catalysts. See L. Resconi et al, Macromolecules, 1990 (23), 4489-4491.

It is considered that the present invention can be applied to any of the above discussed aluminoxanes. Aluminoxanes are generally obtained commercially in the form of hydrocarbon solutions,
generally aromatic hydrocarbon solutions, since the
more active higher molecular weight aluminoxanes are
generally insoluble in aliphatic hydrocarbons. Unless
these samples have been subjected to special treatment,
they typically contain trialkylaluminum as well as the
oligomeric aluminoxane. The trialkyl aluminums
generally include those in which the alkyl groups
contain 1 to 8 carbon atoms, most generally, one to two
carbon atoms. Preferably, the trialkylaluminum
consists essentially of trimethylaluminum.

The present invention is particularly useful
for modifying aluminoxane solutions containing both
trialkylaluminums and aluminoxanes, particularly the
aluminoxanes wherein n of the above formula is at least
about 2 and m is at least about 3, and even more
preferably wherein n and m are both greater than 4.
The preferred aluminoxanes for use in the present
invention are those in which R of the above formulas is
methyl or ethyl, preferably methyl. Preferably, the
organo-aluminoxane is a hydrocarbyl-aluminoxane which
consists essentially of methylaluminoxane or
ethylaluminoxane.

Various boroxines are known in the art. The
term organo-boroxine as used herein refers to compounds
of the formula (RBO)_3 wherein each R is the same or a
different organo group free of hydroxyl (HO-) or
mercapto (HS-) groups. The R groups could include such
radicals as methyl, ethyl, isopropyl, tertiary butyl,
2-ethyl ethylene, tri-n-butyl methyl, o-tolyl, phenyl,
o-tri-fluoro methyl phenyl, o-chloro-phenyl, 2,6-
dimethyl phenyl, C2H5-S-CH2CH2CH2-, CH2=CF-CH2-, α-
naphthyl, β-naphthyl, and the like. The R groups could
also be R'O-, R'S-, R'2N-, R'2P-, and R'3Si- wherein
each R' is a hydrocarbyl group. Generally each R group
contains about 1 to about 25 carbon atoms, more
typically 1 to 10 carbon atoms. Especially preferred
are the hydrocarbyl boroxines and the hydrocarbyl oxy
boroxines. Examples of hydrocarbyl boroxines include trimethyl boroxine, triethyl boroxine, tri-n-propyl boroxine, tributyl boroxine, tricyclohexyl boroxine, triphenyl boroxine, methyl diethyl boroxine, dimethylethyl boroxine, and the like. The currently preferred hydrocarbyl boroxines are trimethyl boroxine and triethyl boroxine. The term hydrocarbyloxy boroxine refers to compounds of the formula \((R'\text{O})_3\text{BO}\) wherein each \(R'\) can be the same or different hydrocarbyl group, generally containing about 1 to about 10 carbon atoms. Trialkyloxy boroxines are currently preferred. Trimethoxy boroxine is an example. Preferably, the organo-boroxine consists essentially of methylboroxine, methoxyboroxine, or trimethoxyboroxine. By use of the term "consists essentially of" it is intended that the organo-aluminoxane, the trialkylaluminum and the organo-boroxine do not include any components which would materially affect the desired properties provided to the solid organo-aluminoxy product produced by the process of the invention.

The reaction of the boroxine with the aluminoxane can be carried out in any suitable manner. One particularly desirable technique simply involves contacting the two reactants in a suitable liquid diluent. One preferred technique involves contacting a hydrocarbon solution of the aluminoxane with a hydrocarbon solution of the boroxine. Another technique involves contacting a hydrocarbon solution of the aluminoxane with a countersolvent to produce a slurry comprising soluble aluminoxane and insoluble particulate aluminoxane and then contacting the resulting slurry with a solution of the boroxine. It is also within the scope of the present invention to carry out the reaction of the boroxine and the aluminoxane in the presence of a particulate diluent so that the insoluble product becomes deposited upon the
particulate diluent. Typical particulate diluents would include such inorganic materials as silica, alumina, aluminum phosphate, silica-alumina, titania, kaolin, fumed silica, and the like.

It is also within the scope of the present invention to prepare the inventive particulate organo-aluminoxy composition and then combine it with a solution of a trialkylaluminum compound, e.g. trimethylaluminum or others of the type mentioned above, and then to contact the resulting slurry with additional boroxine of the type described above. It is believed that this process may provide a method for further increasing the molecular weight of the particulate aluminoxy composition that is initially produced by reacting the aluminoxane with the boroxine. Obviously, such a process could be repeated several times to obtain the desired level of molecular weight, particle size, bulk density, or other characteristic that is desired for a particular application.

The amount of boroxine employed relative to the aluminoxane can vary over a wide range depending upon the particular results desired. A technique which has been used in this invention for reflecting the ratio of boroxine to aluminoxane, involves the use of a calculated amount for the amount of aluminoxy aluminum in the aluminoxane solution. As used herein the term calculated aluminum is the value obtained by using a vacuum to strip the solvent off a known volume of the aluminoxane solution; weighing the recovered solid; and dividing the weight of the solid per milliliter by the average molecular weight of the aluminoxy units, i.e. 58 for methylaluminoxane, so that one obtains a calculated value for the number of moles of aluminum per volume of the aluminoxane solution that is to be
reacted with the boroxine. It is theorized that a substantial portion of any free trihydrocarbyl aluminum in the aluminoxane solution is removed when the solvent is stripped off. Any trihydrocarbyl aluminum that is present in the solid recovered after the vacuum stripping, is not considered to have a significant effect upon the calculated aluminum value. Using this method, the atomic ratio of the boron in the boroxine to calculated Al in the aluminoxy units of the aluminoxane employed will be in the range of about 1/20 to about 1/3, more preferably about 1/15 to about 1/5, still more preferably about 1/7. As noted above, the commercial aluminoxane solutions generally contain at least some trihydrocarbyl aluminum, in addition to aluminoxy units. Generally, the trihydrocarbyl aluminum accounts for about 0.1 to about 35 weight percent of the aluminum in the solution. It is generally preferred for the boroxine to be employed in such an amount that the molar ratio of the boroxine to the trihydrocarbyl aluminum be at least about 0.3334/1.

In view of the demonstrated activity of the boroxine precipitated organo-aluminoxy products of the present invention, it is considered that such solid organo-aluminoxy products will be suitable as replacements for soluble aluminoxy products in polymerization reactions. Accordingly, the inventive solid aluminoxanes should be suitable as catalyst components with any number of the transition metal-containing olefin polymerization catalysts that have in the past been employed with soluble aluminoxanes. Some examples of such transition metal-containing catalysts are disclosed in the previously mentioned U.S. Patent 3,242,099. The use of more than one such catalyst is also within the scope of the present invention. In a preferred embodiment, the catalyst portion of the catalyst system is selected from transition metal compounds of metals of Groups IVB, VB, and VIB.
Examples of the transition metals thus include zirconium, titanium, hafnium, and vanadium. Such compounds can be represented by the formula $\text{MX}_n$ wherein $M$ represents the transition metal atom and $X$ represents a halogen atom or an organo group, and $n$ is the valence state of the transition metal. Some illustrative examples of such transition metal compounds include vanadium dichloride, vanadium trichloride, vanadium tetrachloride, vanadium pentafluoride, vanadium triiodide, titanium dibromide, titanium tetrachloride, titanium trichloride, titanium tetrafluoride, titanium tetraiodide, titanium tetrabromide, zirconium trichloride, zirconium tetrachloride, chromic chloride, titanium tetraethoxide, titanium tetrabutoxide, zirconium tetrabutoxide, dicyclopentadienyl titanium dichloride, dicyclopentadienyl zirconium dichloride, chromium (III) 2-ethylhexanoate, and the like.

In a particular preferred embodiment the transition metal catalyst component comprises a metallocene. Examples of metallocenes include compounds of the formula $\text{ML}_x$ wherein $M$ is the transition metal, at least one $L$ is a ligand coordinated to the transition metal compound having an alkyldienyl skeleton, the other $L$'s can be selected from ligands having alkyldienyl skeletons, hydrocarbon radicals having 1 to 12 carbon atoms, alkoxy radicals having 1 to 12 carbon atoms, aryl oxy radicals having 6 to 12 carbon atoms, halogen, or hydrogen, and $x$ is the valence of the transition metal.

The term "alkyldienyl skeleton" is intended to include such ligands as cyclopentadienyl, alkyl-substituted cyclopentadienyl compounds such as methyl cyclopentadienyl, ethyl cyclopentadienyl, n-butyl cyclopentadienyl, dimethyl cyclopentadienyl, pentamethyl cyclopentadienyl, and the like. Other examples of such cycloalkyldienyl ligands include substituted and unsubstituted indenyls or fluorenlyls,
tetrahydroindenyls, and the like. Examples of such metallocenes are disclosed in U.S. Patent 5,091,352. Some specific examples include bis cyclopentadienyl zirconium dichloride, bis(methylcyclopentadienyl) zirconium dichloride, and bis(n-butyl cyclopentadienyl) zirconium dichloride.

It is also within the scope of the present invention to have two of the L groups be cycloalkyldienyl-type groups which are bonded together by a suitable bridging group. Some such metallocenes are referred to in the art as sandwich-bonded metallocenes. The term "sandwich-bonded metallocenes" is used to indicate that the metal of the metallocene is sandwiched between two opposed cycloalkyldienyl portions of the bridged ligand. Some examples of such bridged ligands include 1-(9-fluorenyl)-1-(cyclopentadienyl) methane, fluorenyl cyclopentadienyl dimethyl methane, 1,2-bis-indenyl ethane, and the like. Metallocenes also include so-called "half-sandwich-bonded", i.e. those in which only one of the cycloalkyldienyl portions is bonded to the metal. An example would be (1-fluorenyl-1-cyclopentadienyl methane) zirconium trichloride.

It is also within the scope of the present invention to employ the inventive solid aluminoxy product in combination with the third generation supported high activity transition metal containing olefin polymerization catalysts. Some examples of typical high activity solid transition metal containing olefin polymerization catalysts include those disclosed in U.S. Patent Nos. 4,326,988 and 4,394,291.

It is also within the scope of the invention to prepare a prepolymerized solid catalyst composition by combining the transition metal component and the inventive solid aluminoxy composition and conducting prepolymerization of an olefin to produce an active prepolymerized solid which is later used in a
polymerization zone.

The particular polymerization conditions employed using the inventive compositions can vary depending upon the particular results desired. It is considered that the inventive solid organo-aluminoxy product can be employed in solution, suspension, and gas phase polymerization of a wide range of olefinically unsaturated monomers. The ratio of the transition metal catalyst to the inventive solid aluminoxy product can vary widely depending upon the particular catalyst selected and the results desired. Typically, the atomic ratio of aluminum in the inventive aluminoxy product to the transition metal is in the range of about 1/1 to about 5000/1, preferably about 15/1 to about 1000/1, and more preferably about 100/1 to about 1000/1. For a particular transition metal catalyst it is considered that polymerizations can be carried out under the same conditions as would be suitable for prior art aluminoxanes.

Examples of some monomers for polymerization include ethylene and alpha-olefins having 3 to 20 carbon atoms, such as propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, 1-octene, 1-hexadecene, cyclopentene, norbornene, styrene, 4-methyl styrene, vinyl cyclohexane, butadiene, and the like and mixtures thereof.

The present invention is particularly useful in slurry type polymerizations since it allows one to carry out such polymerizations more effectively than has heretofore been possible. A particularly preferred type of slurry polymerization involves the continuous loop reactor type polymerization wherein monomer, feed, catalyst, and diluent, if employed, are continuously added to the reactor as needed and polymer product is continuously or at least periodically removed.

The inventive organo-aluminoxy product has been demonstrated to be effective as a cocatalyst in
the continuous loop slurry type polymerization with metallocene catalysts for the production of polyethylenes having a broad range of properties. Generally in such processes, ethylene is polymerized in the presence of a suitable liquid diluent, a higher alpha-olefin comonomer, and optionally, hydrogen. The polymerization temperature can vary over the range which will allow for slurry polymerization. Often the slurry polymerization would be conducted at a temperature in the range of about 60°C. to about 100°C., although higher and lower temperature can be used. The employment of hydrogen in such a continuous loop polymerization using the inventive cocatalyst has been demonstrated to provide very interesting effects, specifically, broad molecular weight distribution. Polyethylenes of broader molecular weight distribution are produced by introducing only enough hydrogen to produce the desired melt index without reducing the molecular weight distribution. This is particularly surprising in that in the past, metallocene polymerizations employing a single metallocene catalyst have generally given narrow molecular weight distribution products, for example products having a molecular weight distribution in which the ratio of the weight average molecular weight to the number average molecular weight is in the range of about 2 to 3. In contrast, by using the correct conditions with the inventive solid aluminox product, it is possible in a slurry polymerization to produce polyethylene in which the ratio of the weight average molecular weight to the number average molecular weight is as high as 21 or more.

A further understanding of the present invention and its objects and advantages will be provided by referring to the following examples.

Example I
A toluene solution of methylaluminoxane
obtained from Schering was reported to contain about 30 weight percent of methylaluminoxane (herein also referred to as MAO) based on a total weight of the solution. Drying a 2 ml portion of that commercial solution in vacuo at room temperature yielded 0.57 grams of solid. Figure 1 shows the infrared spectrum of such a solid in nujol.

While being stirred, a 20 ml portion of the Schering 30 weight percent MAO/toluene solution had about 50 ml of decane added. The decane had been dried over molecular sieves. The resulting mixture was cloudy. It was removed from the dry box and evacuated. The solution was stirred at 35°C. for 3 hrs. under a vacuum. The white slurry was returned to the dry box and filtered and then the solids were dried in vacuo. A yield of 2.69 grams of a colorless solid was obtained. It is thus estimated that more than half of the methylaluminoxane remained in the liquid. The inventors theorize that this decane soluble MAO may have been responsible for at least some of the adverse effects that were noted when an attempt was made to carry out a metallocene catalyzed ethylene polymerization under particle form conditions using the commercial MAO.

Then 0.1 gram of methylboroxine was dissolved in 1 ml of toluene. The resulting toluene solution was added dropwise to a 20 ml aliquot of the filtrate, i.e. the decane soluble MAO. Immediately upon addition of the methylboroxine solution, copious white solids appeared. After stirring for 1 hr. the solids were collected on a filter, washed with 10 ml of hexane and dried. About 0.47 grams of solids were recovered.

A 0.23 gram portion of the solids produced from the methylboroxine reaction was slurried in 5 ml of decane. Then 10 mg of bis(cyclopentadienyl)zirconium chloride was dissolved in 1 ml of toluene and the resulting solution was added
to the decane slurry. The slurry was stirred for 1 hr. and yielded a brown solid phase and a colorless solution phase. The solid phase is referred to herein as Catalyst System A.

The resulting solid metallocene catalyst system was then evaluated for activity in the polymerization of ethylene under particle form conditions. The polymerization was conducted at about 70°C. in 2 liters of isobutane in the presence of hydrogen in an autoclave reactor. The partial pressure of the isobutane and hydrogen was about 175 psi and the partial pressure of the ethylene was about 380 psi. The polymerization was carried out for 1 hr. and yielded 224.4 grams of dry polymer having a melt index of 0.48 and a high load melt index of 10.28. The bulk density was 23.4 gms/100 ml. The reactor was easy to clean up. There was minimal fouling or coating of polymer on the reactor. The fouling observed with Catalyst System A was significantly less than that observed when a similar polymerization was carried out using the same metallocene with the commercial MAO/toluene as a cocatalyst.

Example II

In this case, a methylaluminoxane obtained from Ethyl Corporation was evaluated. The methylaluminoxane product was a solution in toluene. The weight percent MAO in the toluene solution was reported by the manufacturer to be about 10 weight percent. The product was also reported to have an aluminum content of about 4.2 weight percent. About 22 weight percent of the aluminum was reported as being considered to be present as trimethylaluminum.

While 10 ml of the commercial MAO/toluene solution was stirred, 25 ml of hexane was added by a syringe. The previously clear toluene solution became cloudy. The slurry was stirred for 1 hr. at 25°C. in a dry box. The solids were collected on a filter and
dried. About 0.142 grams of solid was recovered which is considered to be about 15 weight percent of the methylaluminoxane in the original slurry.

The resulting solid methylaluminoxane was added to 10 ml of mixed hexanes and then a solution formed by adding 4 milligrams of bis(cyclopentadienyl)zirconium dichloride to toluene was combined with the hexane slurry. The solid turned pale yellow.

This catalyst was then evaluated for the particle form polymerization of ethylene using conditions of the type described for Example I. The 1 hr. polymerization yielded 235.3 grams of dry polymer. The polymer had fairly good particle form but the reactor had significant fouling and was hard to clean up. A hot wash with toluene was required to remove material coating the reactor. This demonstrates that even though countersolvent precipitation resulted in a solid product, that product still resulted in reactor fouling.

**Example III**

An experiment was carried out by adding 25 ml of hexane to 10 ml of the same commercial Ethyl Corporation toluene solution of methylaluminoxane used in Example II. A precipitate formed. Then 2 ml of a hexane solution containing 0.034 grams of methylboroxine was added to the slurry. The slurry was stirred for 1 hr. at 25°C. in a dry box. The solids were collected on a filter and dried. The yield was 0.221 grams which is calculated to be about 22.5 weight percent of the MAO in the commercial solution.

To the filtrate was added 0.4 grams methylboroxine in 2 ml of hexane with vigorous stirring. The solution fumed slightly and copious precipitates were evident. The slurry was stirred for 1 hr. and the solids were collected on a filter. The recovered dried solids weighed 0.55 grams. This is
considered to correspond to about 55.8 weight percent of the total MAO in the commercial solution.

A first catalyst, referred to herein as Catalyst B, was prepared from the solid obtained from the initial precipitation of the commercial MAO solution with methylboroxine. That catalyst preparation involved slurring 0.221 grams of the boroxine precipitated MAO in 10 ml of hexane and then adding 3 ml of a toluene solution containing 6 milligrams of bis(cyclopentadienyl)zirconium dichloride. The slurry was stirred for 1 hr., filtered, and dried.

Another catalyst, referred to herein as Catalyst C, was prepared employing 0.22 grams of the solid obtained by the methylboroxine treatment of the filtrate. The catalyst preparation was the same, namely, 3 ml of a toluene solution containing 5 milligrams of bis(cyclopentadienyl)zirconium dichloride was added to a 10 ml hexane slurry of the solid. The solids were collected on a filter and dried.

The two catalysts were then evaluated in the polymerization of ethylene using particle form polymerization conditions analogous to those used in Example I and II. The catalysts were both as active as the catalysts produced from the catalysts prepared by merely precipitating the MAO using hexane. There was however significantly less fouling of the reactor with Catalysts B and C than with the catalyst of Example II, i.e. where the catalyst was prepared from the solid MAO obtained by merely contacting the commercial product with a countersolvent.

Example IV

A series of experiments were carried out to evaluate the effect of the boroxine level on the yield of the inventive solid methylaluminoxane product. The experiments involved, in each case, the use of 5 ml of a methylaluminoxane obtained from Ethyl Corporation and
calculated to have 1.7 moles of aluminoxide units per liter based on evaporating the commercial aluminoxide solution at room temperature under a vacuum and then dividing the weight per liter by 58, the molecular weight of one methyl aluminoxide unit. Each 5 ml portion of the MAO solution had 25 ml of hexane added to it. The slurry was then stirred for 1 hr. Then a known amount of trimethylboroxine was added, in all but one experiment, and the slurry stirred for another hour. The solids were collected on a filter, dried in a dry box, and weighed.

Each of the solids obtained were then used to prepare a catalyst system and evaluated for the particle form polymerization of ethylene. In each catalyst preparation a weighed amount of the aluminoxide solid was slurried in 15 ml of hexane and then a toluene solution of bis(cyclopentadieny1) zirconium dichloride was added. The toluene solution of the metallocene contained about 2 mg of the metallocene per milliliter. In each case, the resulting slurry was stirred, the solids collected on a filter, dried, and weighed.

The catalysts were then evaluated for polymerization activity by polymerizing ethylene under particle form conditions. The conditions involved a total pressure of 450 psi, the partial pressure of the isobutane diluent was 160 psi, and the polymerization was carried out at about 70°C. in 2 liters of the isobutane diluent in the presence of hydrogen. The results of the solid MAO precipitations and the results of the polymerizations using catalysts prepared from those precipitated MAOs are set forth in Table I.
<table>
<thead>
<tr>
<th>Run No.</th>
<th>(MeBO)3 gm</th>
<th>Al*/B</th>
<th>Yield Solid MAO, gm</th>
<th>Yield PE, gm</th>
<th>Activity gm PE/gm catalyst hr.</th>
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</thead>
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</tr>
<tr>
<td>5</td>
<td>0.050</td>
<td>7.3</td>
<td>0.514</td>
<td>70.0</td>
<td>548</td>
</tr>
<tr>
<td>6</td>
<td>0.072</td>
<td>5</td>
<td>0.51</td>
<td>36.2</td>
<td>282</td>
</tr>
<tr>
<td>7</td>
<td>0.180</td>
<td>2</td>
<td>0.650</td>
<td>trace</td>
<td>--</td>
</tr>
</tbody>
</table>

*Calculated Al in aluminoxy units of aluminoxane.
The data reveals that approximately 100% of the MAO is recovered as a solid when the total aluminum to boron ratio is approximately 7.3/1. All the solids with the exception of that produced in Run 7, yielded active ethylene polymerization catalysts when combined with the metallocene. The activity value is based on the total catalyst system, i.e. the solid catalyst resulting from the combination of the solid aluminoxy product and the metallocene.

Example V

A larger scale preparation of the inventive solid aluminoxy product was carried out using a 30 weight percent MAO toluene solution obtained from Schering. In this case, 50 ml of the MAO solution was combined with 200 ml of hexane in a dry box with vigorous stirring. The colorless homogeneous toluene solution turned milky white. The slurry was stirred vigorously for 2 hrs. Then to the above slurry was added dropwise a 50 ml hexane solution of methylboroxine to give 1.4 gm or 33.5 millimoles of methylboroxine. This also translates to calculated aluminum to boron ratio of 7.5 to 1. The complete addition took 1 1/2 hrs. The thick, milky slurry was stirred an additional 3 hrs. and the resulting solid was collected on a filter and dried. A yield of 15.1 gm of solid was obtained which is considered to be about 100% of the MAO in the starting commercial solution.

Example VI

In this example, trimethoxyboroxine rather than methylboroxine was employed as the precipitating agent. In this case, a 10 ml solution of methylaluminoxane in toluene was used that had been obtained from Ethyl Corporation, the methylaluminoxane solution was believed to be 1.7 molar in regard to methylaluminoxane. Here 50 ml of hexane was added to 10 ml of the methylaluminoxane solution. The clouded
slurry was stirred for 1 hr. then a 1 ml toluene solution of trimethoxyboroxine containing 0.131 gm of the boroxine was added dropwise to the slurry. The resulting slurry was then stirred for an additional hour at room temperature. The solids were collected on a filter and dried in a dry box. 1 gram of solid dry product was obtained.

The solid was screened through an 80 mesh sieve and then subjected to MAS NMR analysis using a Bruker/IBM WP200 NMR spectrometer operating at 50.32 MHz for $^{13}$C analysis using a Chemagnetics MAS probe with 7 mm zirconia rotors spinning at 6-7 KHz. Hexamethylbenzene was used as a secondary chemical shift reference to TMS. Figure 3 shows the resulting $^{13}$C-NMR spectra for the solid obtained using trimethoxyboroxine. The spectra shows that in addition to the broad peak centered at about -8.9 ppm which is due to the MAO, a smaller peak was present at about 51.8 ppm which is attributed to methoxy groups. This spectra indicates that the solid product obtained by using trimethoxyboroxine contains methoxy groups. A $^{13}$C-NMR spectra on the solid resulting from the vacuum stripping of a MAO solution was also made. See Figure 4. This spectra does not reveal a peak at 51.8 ppm, i.e. the methoxy peak.

A "B-NMR spectroanalysis was also carried out using BPO$_4$ as a reference. The BPO$_4$ reference alone has a spectrum containing a relatively narrow line referenced at 0 ppm with spinning sidebands on both sides. The spectrum of the inventive trimethoxyboroxine precipitated aluminoxane contained a broad peak centered about 0 ppm with broad sidebands on both sides. This is certainly evidence that the inventive methoxyboroxine-precipitated aluminoxane product contains boron. This is in contrast to the results obtained using methylboroxine rather than methoxyboroxine. When the "B NMR was conducted on
methylboroxine precipitated aluminoxane, the spectra did not reveal the presence of a significant amount of boron.

**Example VII**

A series of precipitations were conducted using various levels of trimethoxyboroxine in combination with a methyl aluminoxane obtained from Schering. A 5 ml portion of the Schering MAO was stripped to dryness to yield 0.33 grams of a solid.

Considerable volatile trimethylaluminum was seen in the trap. Based upon the weight of the solid recovered, it is calculated that the commercial MAO solution was 1.14 molar in aluminoxy aluminum.

The precipitations were conducted by using a solution of trimethoxyboroxine in toluene. The solution was prepared by dissolving 1 gram of the boroxine in 10 ml of toluene. The precipitation was carried out by adding 25 ml of hexane to 5 ml of the commercial MAO solution. The resulting mixture was then stirred 1 hour, and then a specific volume of a 0.01 g/ml trimethoxyboroxine toluene solution was added, the mixture stirred 3 hours, and then the solid was collected by filtration and dried.

The amounts of trimethoxyboroxine employed in the amount of solid aluminoxane obtained is reported in Table II.
Table II

<table>
<thead>
<tr>
<th>Run No.</th>
<th>(MeOBO)₃, ml</th>
<th>Al*/B</th>
<th>Yield Solid MAO, gm</th>
</tr>
</thead>
<tbody>
<tr>
<td>8</td>
<td>0.327</td>
<td>10</td>
<td>0.120</td>
</tr>
<tr>
<td>9</td>
<td>0.49</td>
<td>6.65</td>
<td>0.164</td>
</tr>
<tr>
<td>10</td>
<td>0.55</td>
<td>6.0</td>
<td>0.168</td>
</tr>
<tr>
<td>11</td>
<td>0.61</td>
<td>5.33</td>
<td>0.220</td>
</tr>
<tr>
<td>12</td>
<td>0.71</td>
<td>4.67</td>
<td>0.335</td>
</tr>
</tbody>
</table>

*Calculated Al in aluminoxyl units of aluminoxane.

The activities of the solid aluminoxy product of Runs 11 and 12 were evaluated by slurrying 0.12 grams of the solid aluminoxy product in 25 ml of hexane and then adding a 1 ml toluene solution of 3 mg bis-cyclopentadienyl zirconium dichloride and stirring overnight to obtain a solid catalyst. The solid catalysts were then employed in the polymerization of ethylene using substantially identical conditions. The polymerizations were carried out generally in the manner as described in Example IV. The catalyst system produced using the solid aluminoxane of Run 11 was more active than the catalyst system produced using the solid aluminoxane of Run 12. It is theorized that the solid aluminoxane loses some of its benefits if the level of boroxine is too high. Similar results were noted for the methyl boroxine precipitated aluminoxane in the above Table I.

Example VIII

Another series of methoxy boroxine precipitated aluminoxy products was prepared from a 10 wt. % methylaluminoxane solution in toluene obtained from Schering. The procedure involved adding 75 ml of hexane to 10 ml of the commercial MAO solution and stirring for 1 hr. Then a toluene solution of the
trimethoxyboroxine was added, when employed. The trimethoxyboroxine solution that was employed was prepared by adding 1 gram of trimethoxyboroxine to 10 ml of toluene. The slurry was then stirred for three more hours and the solids collected and dried. Catalysts were prepared by adding 2 ml of a 3 mg/ml toluene solution of bis-cyclopentadienyl zirconium dichloride to a slurry prepared by adding 0.25 grams of the solid MAO in 30 ml of hexene. The slurries were stirred overnight. The solids were collected on a filter and dried to yield the supported catalyst system.

The catalysts were then each evaluated for their effectiveness in the polymerization of ethylene under comparable conditions. The conditions involved a total pressure of about 341 psi in 2 liters of isobutane. The polymerization was carried out at about 70°C. in the presence of hydrogen. The results of the solid MAO precipitations and the results of the polymerizations using the catalysts prepared from those solid MAOs are set forth in Table III.
<table>
<thead>
<tr>
<th>Run No.</th>
<th>(MeOBO)\textsubscript{3} mmol</th>
<th>Al*/B</th>
<th>Solid MAO gm</th>
<th>Yield PE, gm</th>
<th>Activity gm PE/gm catalyst</th>
</tr>
</thead>
<tbody>
<tr>
<td>13</td>
<td>2.5</td>
<td>9</td>
<td>0.46</td>
<td>144.2</td>
<td>1419</td>
</tr>
<tr>
<td>14</td>
<td>2.8</td>
<td>8</td>
<td>0.53</td>
<td>49.3</td>
<td>433</td>
</tr>
<tr>
<td>15</td>
<td>2.7</td>
<td>8.5</td>
<td>0.47</td>
<td>19.7</td>
<td>1461</td>
</tr>
<tr>
<td>16</td>
<td>0</td>
<td>0</td>
<td>0.25</td>
<td>18.93</td>
<td>212</td>
</tr>
</tbody>
</table>

*Calculated Al in aluminoxyl units of aluminoxane.
Here again, it is revealed that the aluminum to boron ratio can affect the activity of the resulting catalyst system.

**Example IX**

A commercial ethyl aluminoxane solution in toluene containing about 10 wt. % ethyl aluminoxane and containing about 31 wt. % aluminum was contacted with a hexane solution of methyl boroxine to produce a solid inventive aluminoxy product. Specifically, 50 ml of the commercial ethyl aluminoxane solution was employed and the methyl boroxine/hexane solution was added dropwise in an amount sufficient to add 0.269 grams of methyl boroxine. The mixture gradually became cloudy. It was allowed to sit and then stirred after complete addition of the boroxine. A slurry of the inventive solid ethyl aluminoxy product resulted. A 5 ml portion of the slurry was combined with 10 ml of a solution of bis n-butylicyclopentadienyl zirconium dichloride containing 4 mg of the metalloocene. Approximately half of the resulting slurry was withdrawn by a syringe and used in an ethylene polymerization under particle form polymerization conditions. The catalyst was active. After the resulting polymer was dried, it weighed 104 grams and the polymerization was only carried out for one-half hour.

An attempt was made to carry out the same reaction using the commercial ethyl aluminoxane solution rather than the inventive solid ethyl aluminoxane. The yield of polymer was lower and there was a heavy coating of polymer on all the metal surfaces of the reactor. In contrast, in using the inventive solid ethyl aluminoxane there was only a film of polymer on the reactor walls.

**Example X**

The inventive solid ethyl aluminoxy product prepared in the previous example was combined with 0.048 grams of 1-(9-fluorenyl)-1-cyclopentadienyl
methane zirconium dichloride, a sandwich bonded bridged ligand metallocene, dissolved in 5 ml of toluene.

The resulting catalyst system was then evaluated in the homopolymerization of propylene under particle form conditions. The aluminum to zirconium ratio was 1,261. The polymerization was carried out for 60 minutes. The polymerization produced 13,254 grams of polypropylene per gram of metallocene in the hour. The polymer had a melt flow of 89.79, a bulk density of 15.0, a weight average molecular weight of 52,470, a number average molecular weight of 32,224, a heterogeneity index of 1.63, and a density of 0.8931.

A similar propylene polymerization run was carried out using the same metallocene but with the commercial ethyl aluminoxane solution rather than the inventive methyl boroxine precipitated aluminoxane product. Three different aluminum to zirconium ratios were evaluated, namely ratios of 991, 782, and 577. The highest activity obtained in the polymerizations carried out using the commercial ethyl aluminoxane was 2,737 grams of polymer per gram of metallocene.

Similar evaluations were carried out using inventive methyl boroxine precipitated ethyl aluminoxane products in which the ratio of the aluminum to boroxine was 5:1 in one case, 7.75:1 in another case, and 10:1 in yet another case. These inventive solid aluminoxane products were evaluated in the polymerization of propylene by preparing catalysts using the same methane bridged fluorenyl cyclopentadienyl zirconium dichloride sandwich bonded metallocene. The catalyst resulting from the precipitation using the 5:1 ratio was less active than the one prepared using the 7.75:1 ratio which in turn was less active than the one prepared using the 10:1 ratio. The ratio of the Al to the Zr in these runs was in the range of about 850/1 to 980/1.

Example XI

A large quantity of trimethoxyboroxine
precipitated methyl aluminoxane product was prepared so that the inventive aluminoxane product could be evaluated for ethylene polymerization on a pilot plant scale in a loop reactor. The inventive solid MAO was prepared from a 10 wt. % solution of MAO in toluene obtained from Schering. The procedure employed for preparing large batches involved the following: (1) 6 gallons of hexane was added to a 10 gallon glass-lined reactor. (2) 7.25 lbs. of the commercial 10 wt. % MAO solution was added to the stirred hexanes. (3) The resulting slurry was stirred for 1 hour. (4) 300 ml of a toluene solution containing about 32 grams of trimethoxyboroxane was added over a 1 hr. period with stirring. (5) The resulting slurry was then stirred for an additional 6 hrs. (6) The solids were allowed to settle overnight. (7) About 5 gallons of solvent was decanted. (8) The remaining solids were washed with 1 gallon of hexanes for 1 hr. with stirring. (9) The major portion of the solvent was decanted and the solids were transferred to a carboy for storage. Three such batches were made.

Each of the resulting inventive solid boroxine precipitated aluminoxane products were combined with a hexene solution of bis n-butylcyclopentadienyl zirconium dichloride by adding the metallocene solution to the solid MAO slurry. The resulting slurry was stirred to assure good mixing and the solid allowed to settle and then the solids were transferred to a carboy. The solids were in each case then collected on a filter, dried, and weighed in a drybox. After isolation, each batch of the precipitated metallocene/MAO catalyst system was checked for activity at standard conditions. The catalysts typically contained about 0.3 weight percent zirconium and about 41 weight percent aluminum.

The batches which all proved to be suitably active were then combined to give 225 grams of solid
which was sieved through a 60 mesh screen in a drybox. This sieved solid was combined with 1 liter of hexanes and then used in pilot plant scale particle form loop polymerizations of ethylene. The pilot plant process employed a 23 gallon pipe loop reactor, a flash chamber, and polymer fluff dryer. Most of the runs were made at about 194°F. reactor temperature and 13-14 mole percent ethylene in the flash gas. However, in the runs which were made to produce lower density products, the reactor temperature was closer to about 180°F., 1-hexene was used as comonomer, and the ethylene mole percent in the flash gas was about 7 to about 8 mole percent. Typically the residence time in the pilot plant reactor was nominally 1.25 hrs. For each set of conditions, batches of polymer fluff were produced in the loop reactor and combined to produce a blend corresponding to the product resulting from those particular process conditions. Each blend was then extruded into pellets. The reactor was used for a two week period in preparing these polymer batches without any need for stopping for cleaning due to fouling. A summary of some of the properties of the various polymers made using the inventive catalyst system in the pilot plant loop reactor are set forth in Tables IV and V.
<table>
<thead>
<tr>
<th>Blend</th>
<th>Pellet Values</th>
<th>Unmilled</th>
<th>Bell ESCR</th>
<th>Flex Mod.,</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>MI</td>
<td>Density</td>
<td>Fluff MI</td>
<td>hrs.</td>
</tr>
<tr>
<td>13</td>
<td>7.32</td>
<td>0.9641</td>
<td>11.08</td>
<td>&lt;24</td>
</tr>
<tr>
<td>14</td>
<td>25.05</td>
<td>0.9623</td>
<td>28.32</td>
<td>BOB*</td>
</tr>
<tr>
<td>15</td>
<td>43.17</td>
<td>0.9624</td>
<td>49.91</td>
<td>&lt;24</td>
</tr>
<tr>
<td>16</td>
<td>18.80</td>
<td>0.9504</td>
<td>20.49</td>
<td>BOB</td>
</tr>
<tr>
<td>17</td>
<td>32.88</td>
<td>0.9502</td>
<td>37.21</td>
<td>BOB</td>
</tr>
<tr>
<td>18</td>
<td>38.24</td>
<td>0.9530</td>
<td>39.86</td>
<td>BOB</td>
</tr>
<tr>
<td>19</td>
<td>44.09</td>
<td>0.9537</td>
<td>44.40</td>
<td>BOB</td>
</tr>
<tr>
<td>20</td>
<td>8.21</td>
<td>0.9435</td>
<td>8.15</td>
<td>&lt;24</td>
</tr>
<tr>
<td>21</td>
<td>3.59</td>
<td>0.9378</td>
<td>3.69</td>
<td>&gt;1000</td>
</tr>
<tr>
<td>22</td>
<td>3.66</td>
<td>0.9330</td>
<td>3.82</td>
<td>&gt;1000</td>
</tr>
</tbody>
</table>

*BOB indicates "breaks-on-bending".
<table>
<thead>
<tr>
<th>Blend</th>
<th>MW/MN</th>
<th>IB</th>
<th>MN/1000</th>
<th>MW/1000</th>
<th>MZ/1000</th>
</tr>
</thead>
<tbody>
<tr>
<td>13</td>
<td>21.1</td>
<td>1.284</td>
<td>10.5</td>
<td>220</td>
<td>4375</td>
</tr>
<tr>
<td>14</td>
<td>16.7</td>
<td>1.234</td>
<td>9.7</td>
<td>162</td>
<td>4202</td>
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<td>15</td>
<td>13.3</td>
<td>1.222</td>
<td>8.3</td>
<td>111</td>
<td>3602</td>
</tr>
<tr>
<td>16</td>
<td>11.5</td>
<td>1.089</td>
<td>11.2</td>
<td>128</td>
<td>19,572</td>
</tr>
<tr>
<td>17</td>
<td>8.6</td>
<td>1.105</td>
<td>9.7</td>
<td>83</td>
<td>2866</td>
</tr>
<tr>
<td>18</td>
<td>11.2</td>
<td>1.131</td>
<td>9.2</td>
<td>103</td>
<td>6092</td>
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<td>19</td>
<td>8.1</td>
<td>1.129</td>
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</tr>
<tr>
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<td>16.0</td>
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<td>966</td>
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<td>20.0</td>
<td>67</td>
<td>142</td>
</tr>
<tr>
<td>22</td>
<td>4.2</td>
<td>0.968</td>
<td>18.0</td>
<td>76</td>
<td>822</td>
</tr>
</tbody>
</table>
Blend 13 was the product of ethylene homopolymerization. The subsequent blends 14-22 were the products of copolymerizations which employed 1-hexene as a comonomer with the ethylene. A difference in the ratios of the weight average molecular weight to number average molecular weight, i.e. MW/MN, was observed to be due to the fact that in the polymers having a higher ratio there was a significant tail on the high molecular weight end of the molecular weight distribution. The presence of this tail seems to be a function of the reactor conditions used to produce the various resins, particularly the amount of comonomer employed. Catalyst productivities determined from total burned ash were in the range of 3,664 to 8,793 lbs. of polymer per pound of catalyst were noted, where catalyst refers to the solid catalyst system resulting from the combination of the metallocene and the inventive solid aluminoxy product.
The claims defining the invention are as follows:

1. A process for producing a solid organo-aluminoxy product useful as a catalyst component in the polymerization of ethylene, which comprises contacting a solution of an organo-aluminoxane with a suitable amount of an organo-boroxine under suitable conditions to form said solid.

2. A process according to claim 1, wherein said organoaluminoxane is a hydrocarbylaluminoxane.

3. A process according to claim 2, wherein said hydrocarbylaluminoxane contains at least one unit of the formula

\[
\text{R} - \text{O-}\text{Al}\text{-Al}\text{-O-R}
\]

wherein \( R \) is an alkyl radical having 1 to 8 carbons.

4. A process according to claim 3, wherein said hydrocarbylaluminoxane consists essentially of methylaluminoxane or ethylaluminoxane.

5. A process according to any one of the preceding claims, wherein said solution comprising said organoaluminoxane further comprises a trialkylaluminum.

6. A process according to claim 5, wherein said trialkylaluminum in said solution consists essentially of trimethylaluminum.

7. A process according to claim 5 or 6, wherein said organo-aluminoxane provides at least about 50 mole percent of the total aluminum in the solution that is contacted with said organo-boroxine.

8. A process according to claim 7, wherein said trialkylaluminum provides no more than about 30 mole percent of the aluminum in the solution that is contacted with the organo-boroxine.

9. A process according to any one of the preceding claims, wherein said organo-boroxine consists essentially of methylboroxine, methoxyboroxine or trimethoxyboroxine.

10. A process according to any one of the preceding claims, which further includes contacting said solution comprising said organoaluminoxane with a countersolvent to result in a slurry containing solid organo-aluminoxane and
then contacting said slurry with said organo-boroxine to produce said solid aluminoxy product.

11. A process according to claim 10, wherein a particulate diluent is present when said organo-boroxine is contacted with said slurry.

12. A process according to claim 10 or 11, wherein said organo-boroxine is employed in an amount such that the atomic ratio of the boron in the boroxine to the calculated aluminum of the aluminoxy units in the aluminoxane is in the range of about 1:20 to about 1:3.

13. A process according to any one of claims 10-12, wherein said organo-boroxine is employed as a solution of the organo-boroxine and a liquid that is the countersolvent for the organo-aluminoxane.

14. A process according to any one of claims 10-13, wherein an aliphatic liquid solution of said organo-boroxine is added to said slurry of said organo-aluminoxane.

15. An olefin polymerization catalyst system comprising the solid resulting from the combination of a solid organo-aluminoxy product produced by a process according to any one of the preceding claims as a co-catalyst with at least one transition metal-containing olefin polymerization catalyst.

16. A catalyst system according to claim 15, wherein said at least one transition metal-containing olefin polymerization catalyst is a metallocene.

17. A catalyst system according to claim 16, wherein said metallocene comprises bis(n-butyl cyclopentadienyl)zirconium dichloride.

18. A catalyst system according to claim 15 or 16, wherein said metallocene comprises 1-(9-fluorenyl)-1-(cyclopentadienyl)-methane zirconium dichloride.

19. A process for producing a polymer which comprises contacting at least one olefin under suitable polymerization conditions with a catalyst system according to any one of claims 15-18.

20. A process according to claim 19, wherein said polymerization is conducted under particle form conditions.

21. A process according to claim 20, which is conducted
in a continuous loop reactor.

22. A process according to any one of claims 19-21, wherein said olefin consists essentially of ethylene, said polymerization is conducted in the presence of hydrogen and the polymer produced has a molecular weight distribution such that the weight average molecular weight divided by the number average molecular weight is greater than 10.

23. A process according to any one of claims 19-21, in which propylene is homopolymerized.

24. A solid organo-aluminoxy product which has a $^{13}$C NMR spectra reflecting the presence of methoxy groups.

25. A product according to claim 24, which contains boron.

26. A solid organo-aluminoxy product which has an infrared spectrum in nujol in which the absorption minimums are substantially as shown in Figure 2.

27. A process for producing a solid organo-aluminoxy product substantially as herein described with reference to any of the examples.

28. A solid organo-aluminoxy product when made by a process according to any one of claims 1-14 and 27.

29. An olefin polymerization catalyst system substantially as herein described with reference to any one of the examples.

30. A process for producing a polymer substantially as herein described with reference to any one of the examples.

31. A polymer when made by a process according to any one of claims 19-23 and 30.

32. A solid organo-aluminoxy product substantially as herein described with reference to any one of the Figures in the accompanying drawings.

DATED: 2 February 1994

PHILLIPS ORMONE & FITZPATRICK
Attorneys for:
PHILLIPS PETROLEUM COMPANY
Abstract of the Disclosure

In accordance with the present invention there is provided a new solid aluminoxy composition prepared by reacting aluminoxide with a boroxine. Still further there is provided olefin polymerization catalyst systems incorporating the inventive solid aluminioxy composition. Still further, there is provided processes of polymerization using the inventive solid aluminioxy composition.
FIG. 1
FIG. 2